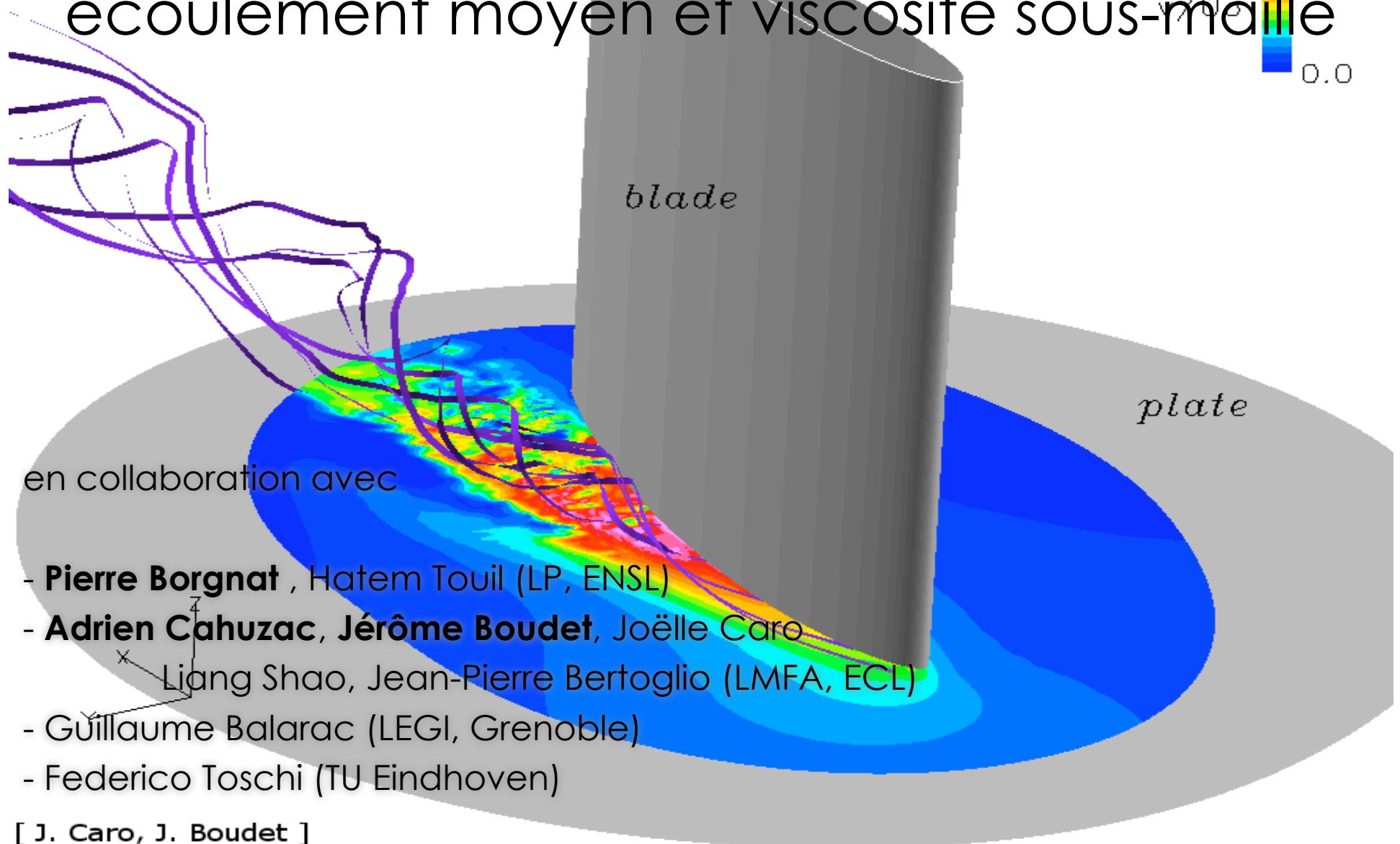
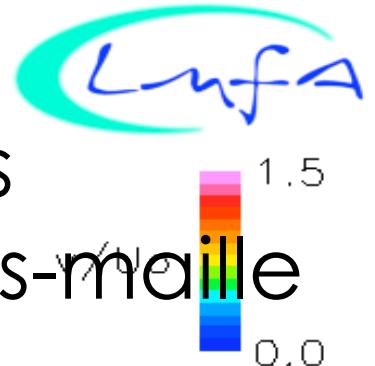


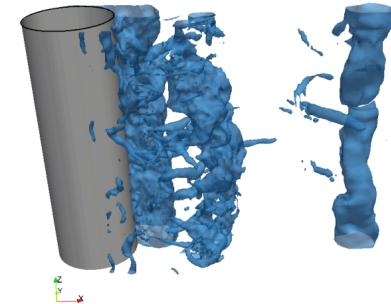
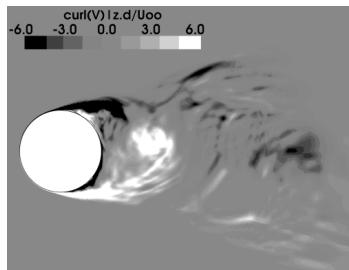
Simulation numérique des écoulements complexes écoulement moyen et viscosité sous-maille



Inhomogénéité - phénoménologie

$u = \langle u \rangle + u'$: décomposition de Reynolds

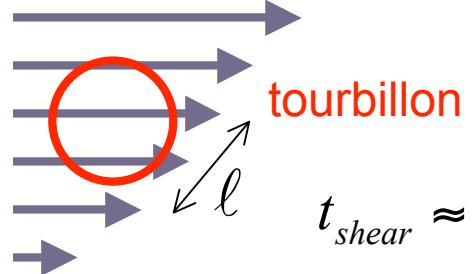
$\Sigma = \sqrt{\langle |\nabla u|^2 \rangle}$: cisaillement



iso-surface: rho=1.16kg/m3

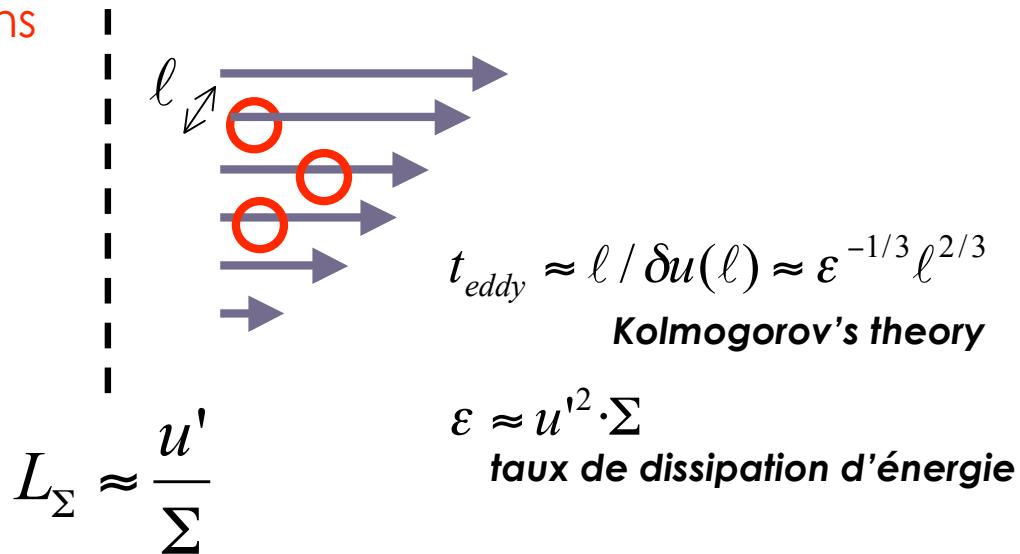
écoulement autour d'un cylindre à
 $Re_D = 47000$ (régime turbulent sous-critique)

écoulement moyen + fluctuations



$$t_{shear} \approx \frac{1}{\Sigma}$$

turbulence cisaillée



turbulence homogène et isotrope

Simulation numérique des écoulements turbulents

goal= get a physically-sound **numerical representation of the flow**

- Direct **Numerical Simulation** (all scales of motion) is usually prohibitive

- **alternatives = partial representation of the flow :**

- **Reynolds-Averaged Navier-Stokes** : mean flow
- **Large-Eddy Simulation** : large-scale dynamics of the flow

→ **Does it make sense (from a physical viewpoint) ?**

→ **What are the governing equations?**

$$\partial_t \tilde{U}_{grid} = \text{NS}(\tilde{U}_{grid}) + \text{div } \boldsymbol{\tau}_{subgrid}$$

$$\boldsymbol{\tau}_{subgrid} - \text{tr}(\boldsymbol{\tau}_{subgrid})\mathbf{I} = -2\nu_{subgrid} \tilde{S}$$

SGS viscosity = property of the flow, not of the fluid... (very) bad news !

$$\nu_{subgrid}(\Delta, \tilde{U}_{grid}, \nabla \tilde{U}_{grid}, \text{etc.})?$$

Effet du cisaillement en équations

$$u_i = u'_i + \frac{\partial \langle u \rangle_i}{\partial x_j} \cdot x_j : \text{ locally uniform shear}$$

- after some (exact) calculations from the Navier-Stokes equations...

$$T_{sgs}(l) = \frac{1}{4\pi l^2} \oint_{\partial B_l} \left(\left\langle |\delta u'(x, l)|^2 \cdot \delta u'_i(x, l) \right\rangle + \frac{\partial \langle u \rangle_i}{\partial x_j} \cdot l_j \left\langle |\delta u'(x, l)|^2 \right\rangle \right) dS_i$$

- in the context of LES :

$$-\langle \tau_{sgs} \cdot \bar{S} \rangle = 2 \langle \nu_{sgs}(\Delta) \cdot |\bar{S}|^2 \rangle \approx T_{sgs}(\Delta)/\Delta \quad \text{with } \Delta = \text{grid spacing}$$

$$\delta u'(\Delta) \approx |\bar{S}'| \cdot \Delta \quad \text{and} \quad \delta U(\Delta) \approx |\langle \bar{S} \rangle| \cdot \Delta \Rightarrow \nu_{sgs}(\Delta) = (C_s \Delta)^2 \cdot (|\bar{S}'| - |\langle \bar{S} \rangle|)$$

Shear-Improved Smagorinsky Model
Lévéque et al., *J. Fluid Mech.* (2007)

$$\nu_{sgs}(\Delta) = (C_s \Delta)^2 \cdot \left(|\bar{S}| - |\langle \bar{S} \rangle| \right)$$

If $|\tilde{S}'| \gg |\langle \tilde{S} \rangle|$: Smagorinsky model for HI turbulence ($C_s = 0.17$)

$$\nu_{sgs} \approx (C_s \Delta)^2 \cdot \frac{\delta u'(\Delta)}{\Delta} \approx (C_s \Delta)^2 \cdot |\tilde{S}'|$$

If $|\langle \tilde{S} \rangle| \gg |\tilde{S}'|$: Shear-dominated SGS viscosity

$$\nu_{sgs} \approx (C_s \Delta)^2 \cdot \frac{|\tilde{S}'|^2}{|\langle \tilde{S} \rangle|}$$

PLUS :

- physically-sound, no ad-hoc parameter
- low computational cost
- easy to parallelize
- convenient for boundary conditions

MINUS :

- requires **estimation of mean-flow as the simulation runs!**

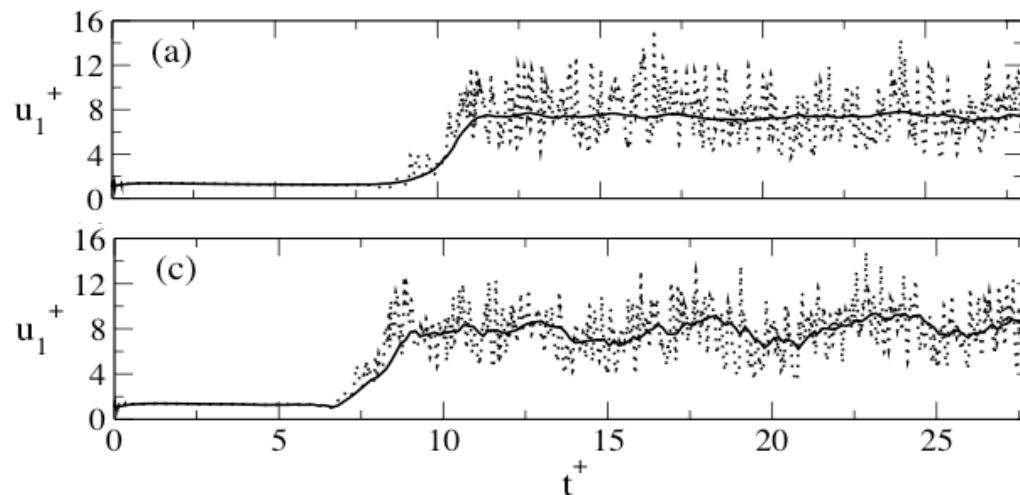
signal processing

Application to complex-geometry unsteady turbulent flows (real-world flows)

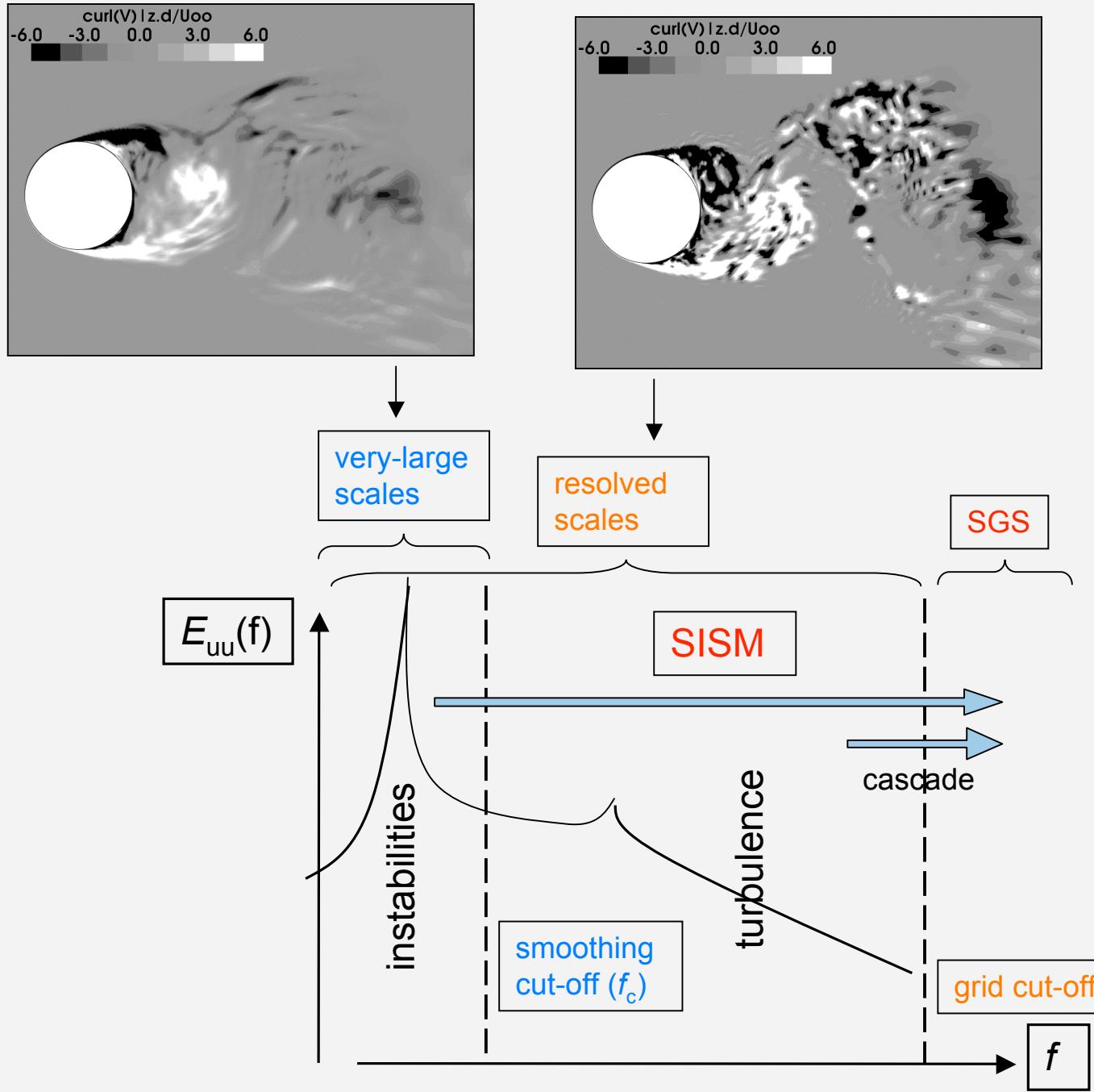
Cahuzac et al., in press Phys. Fluids (2010)

How to extract (or reconstruct) the mean flow as the simulation runs ?

- **physically sound** : smoothing in time
mean flow = low-frequency component of the flow



- manageable** from computational viewpoint : recursive filter
- adaptive** : Kalman filtering



Exponentially-weighted moving average exponential smoothing

$$\langle u \rangle^{(n+1)} = (1 - c_{\text{exp}}) \cdot \langle u \rangle^{(n)} + c_{\text{exp}} \cdot u^{(n+1)} \quad \text{at each grid point}$$

- c_{exp} : smoothing factor

- equivalent to first-order low pass filter with cut-off frequency f_c :

$$c_{\text{exp}} = \frac{2\pi f_c \Delta t}{\sqrt{3}} \approx 3.628 f_c \Delta t$$

PLUS :

- conceptually simple
- local in space
- low memory storage

MINUS :

- uniform physically-sound cut-off frequency ?
- unavoidable phase delay : $\Delta t / c_{\text{exp}}$

Low-pass Kalman filter

adaptive exponential smoothing

- $\langle u \rangle^{(n+1)} = \langle u \rangle^{(n)} + \delta \langle u \rangle^{(n+1)}$: model

control increment = random noise with *fixed variance*

$$\sigma_{\delta \langle u \rangle} = \frac{2\pi}{\sqrt{3}} \cdot f_c \Delta t \cdot u^*$$

$\sigma_{\delta \langle u \rangle} / \sigma_{\delta u} = c_{\text{exp.}}$ for stationary periods

- $u^{(n+1)} = \langle u \rangle^{(n+1)} + \delta u^{(n+1)}$: observation

deviation from the estimated mean = random noise with variance

$$\sigma_{\delta u}^{(n+1)} = \max \left[u^* \cdot \left| \langle u \rangle^{(n+1)} - u^{(n+1)} \right|, 0.1 \cdot u^{*2} \right]$$

predict and update :

$$\langle u \rangle^{(n+1)} = (1 - K^{(n+1)}) \cdot \langle u \rangle^{(n)} + K^{(n+1)} \cdot u^{(n+1)}$$

$K^{(n+1)}$ optimal Kalman gain (given by theory)

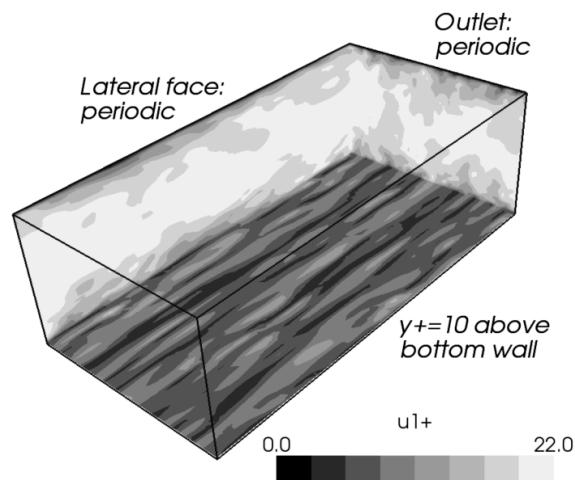
Practical evaluation of the method

Turb'Flow solver (Jérôme Boudet, LMFA):

- Finite volume
- Convective fluxes by centered schemes on four points
- Diffusive fluxes by centered scheme on two points
- SGS model = Shear-Improved Smagorinsky Model (SISM)

Cahuzac et al. Phys. Fluids (2010)

plane-channel Flow at $Re_w = 395$



resolution: $49 \times 89 \times 41$

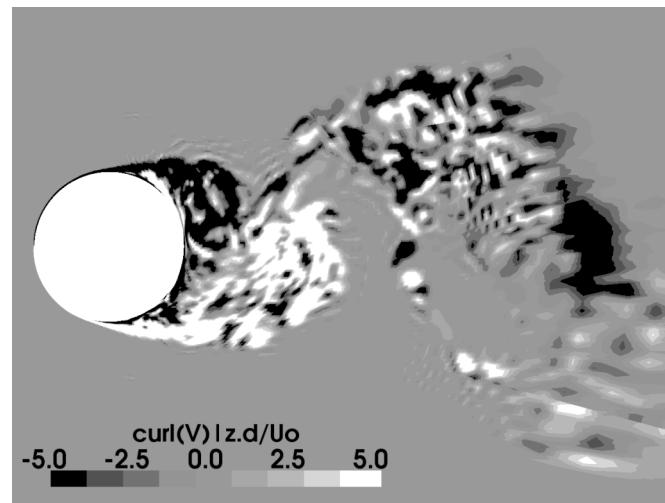
$\Delta x+=52$, $\Delta z+=31$, $\Delta y+=0.5 \dots 24$

$$\boxed{u^* = u_{wall}}$$

friction velocity

$$\boxed{f_c = u^*/\delta}$$

flow past a circular cylinder at $Re_D = 47,000$



3.10^6 mesh-points

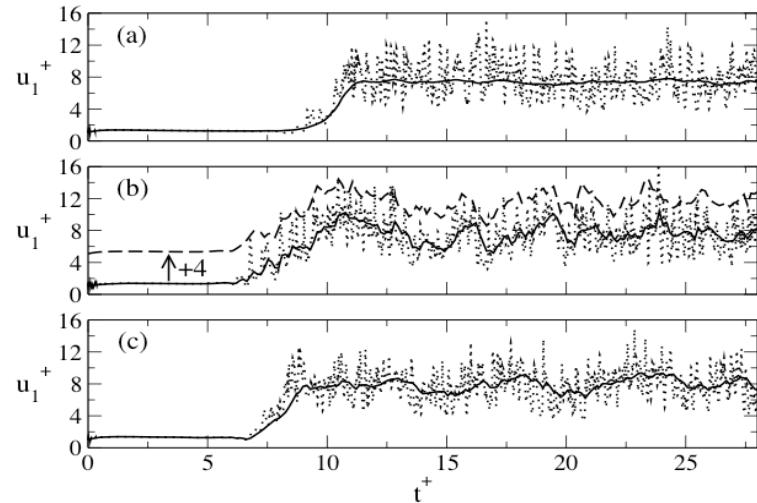
$\Delta r+=1$, $R\Delta\theta+=20$, $\Delta z+=25$

$$\boxed{St = f_s \cdot D/U_\infty}$$

Strouhal number

$$\boxed{f_c = 2f_s}$$

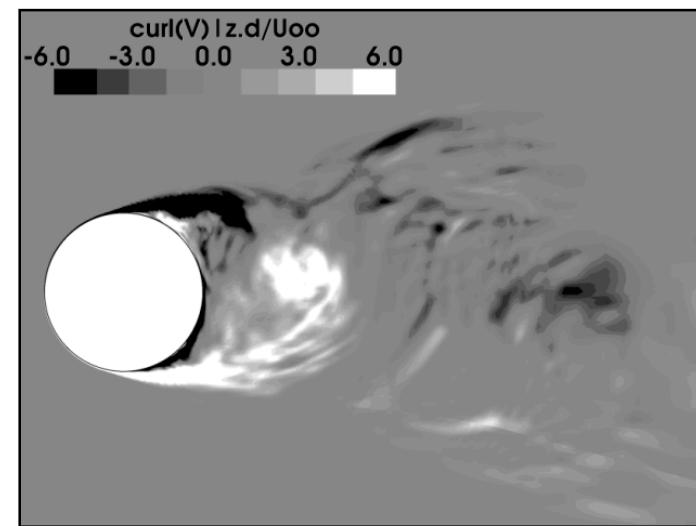
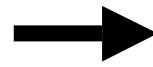
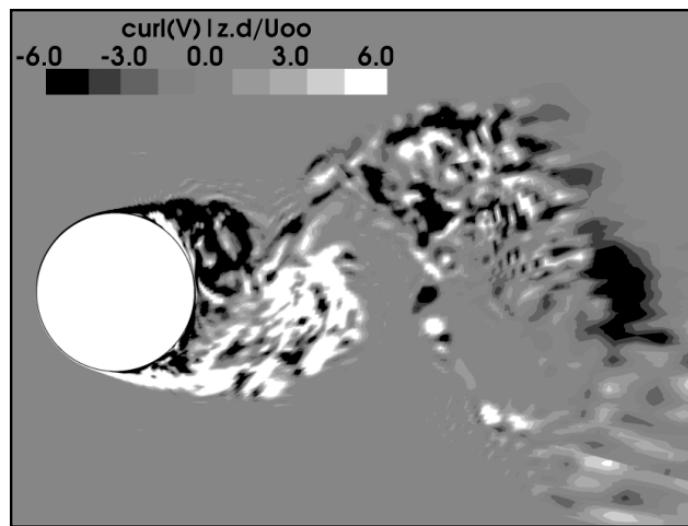
Velocity probes at $y^+=10$ in the plane-channel flow (Rew=395)

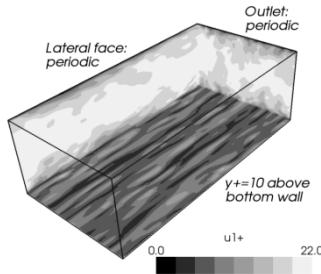


... spatial average (along x-z)

... exponential smoothing compared to
spatial average (along x)

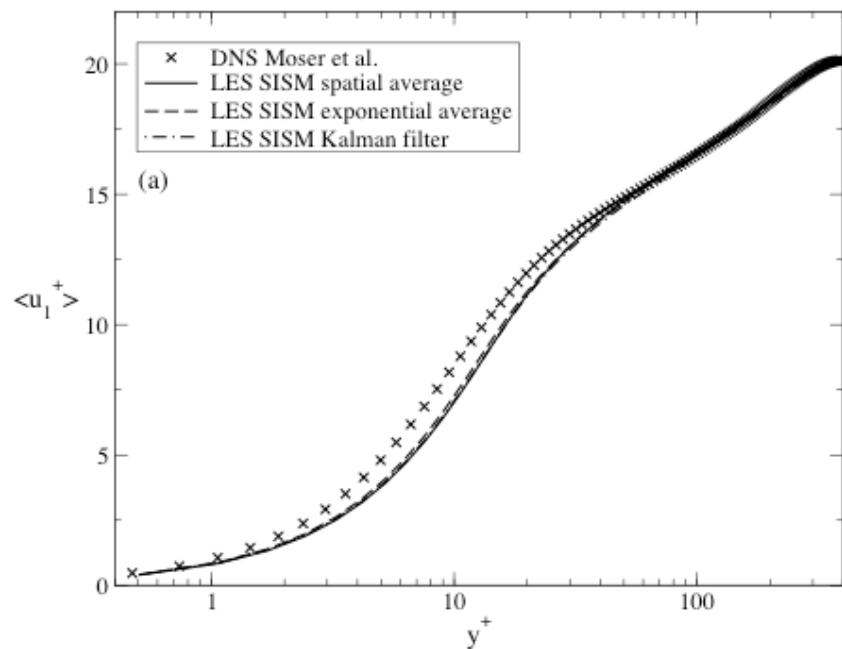
... Kalman filtering



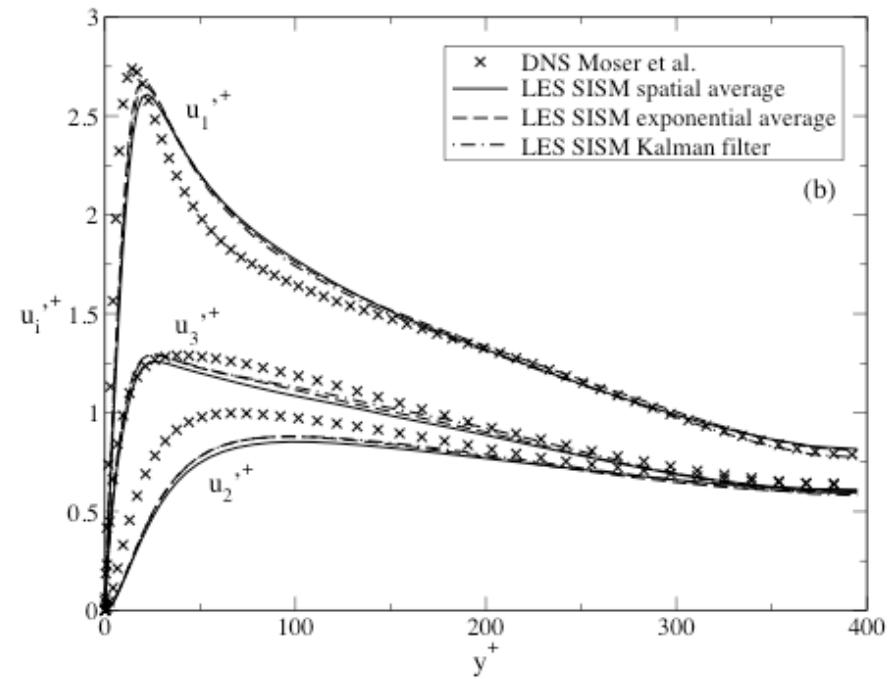


Plane-channel flow

comparisons with DNS data



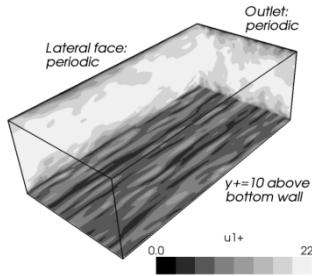
streamwise velocity profile



turbulent intensity profiles

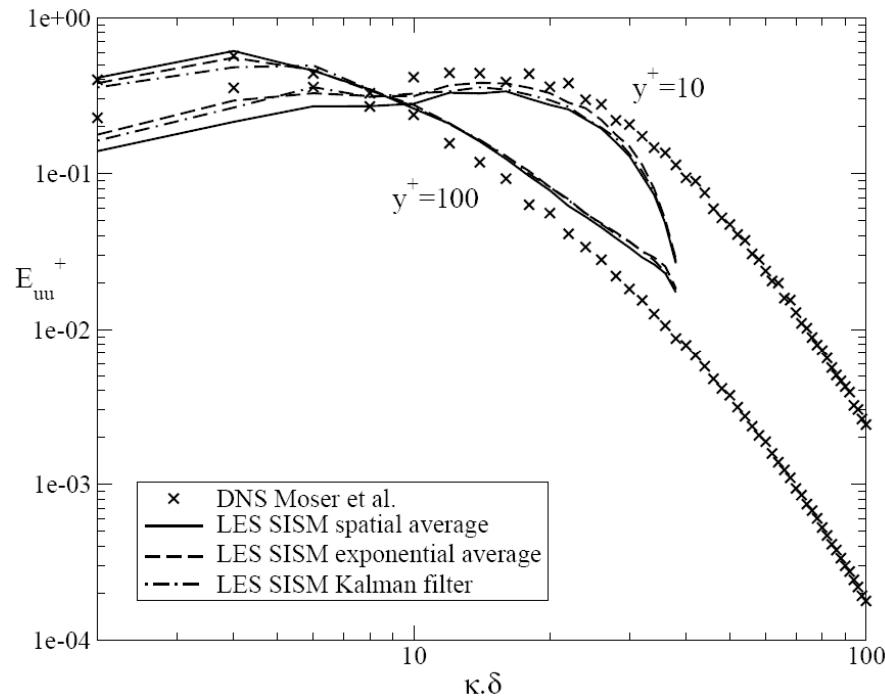
friction velocity: $u_w^{\text{exp.}} = 0.54 \text{ m.s}^{-1}$

$u_w^{DNS} = 0.59 \text{ m.s}^{-1} \rightarrow$ within the 10% level of accuracy
reviewed for standard SGS models

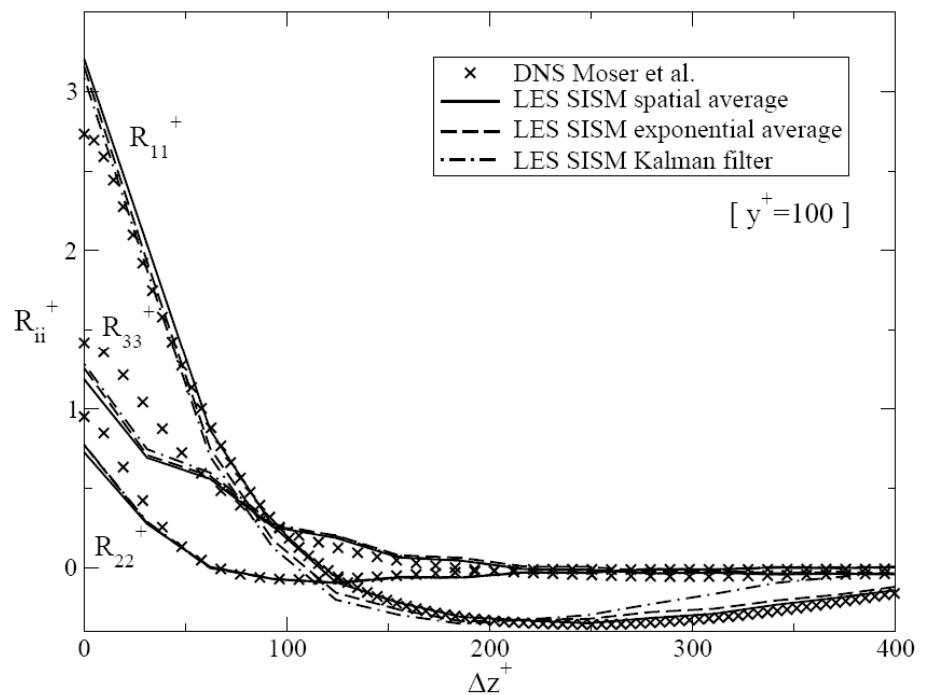


plane-channel flow

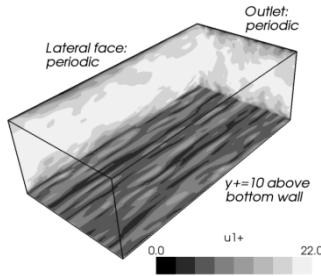
comparisons with DNS data



spanwise spectra
of streamwise velocity

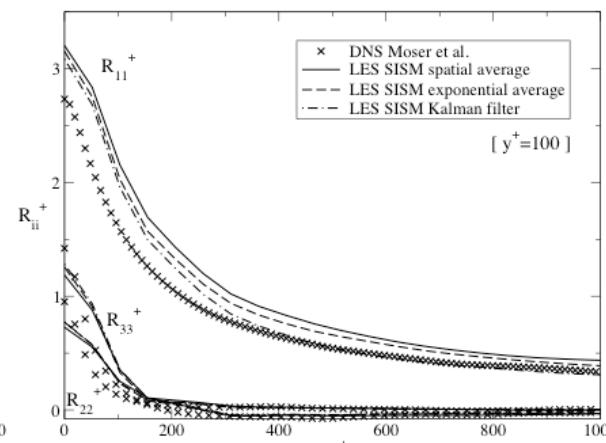
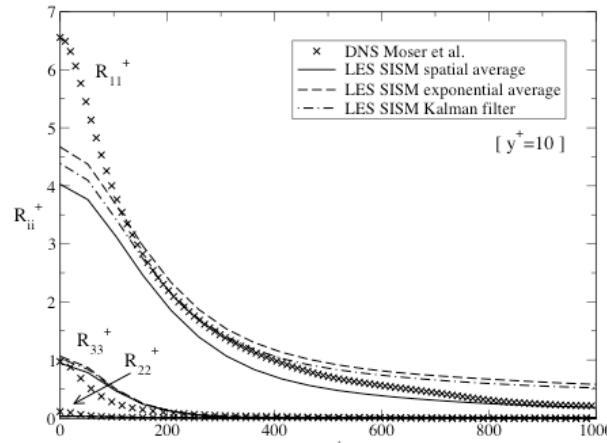


two-point velocity correlation
for spanwise separation

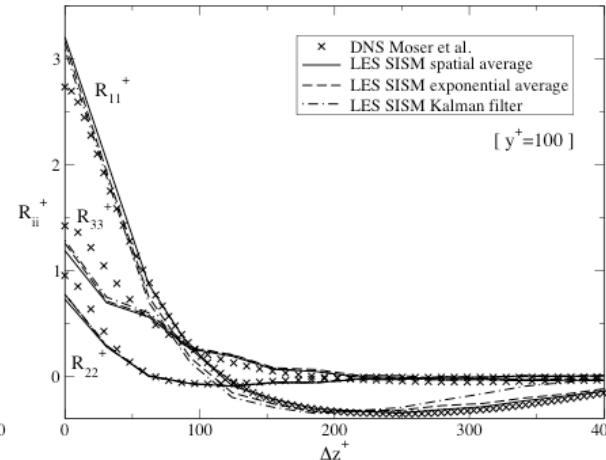
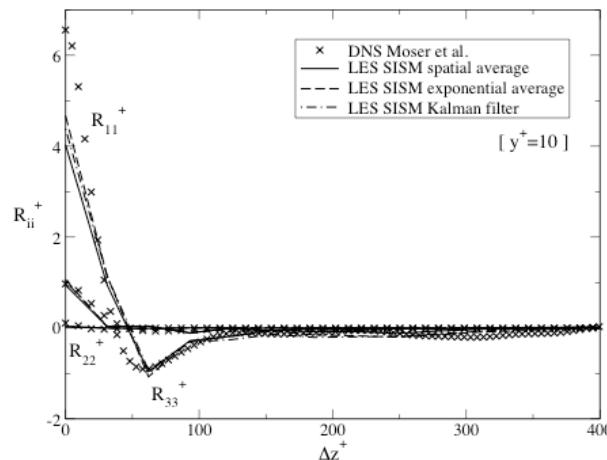


plane-channel flow

comparisons with DNS data

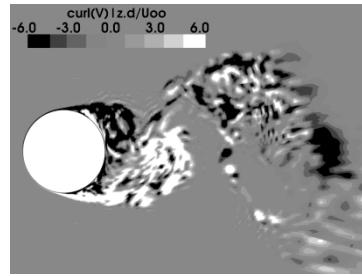


streamwise



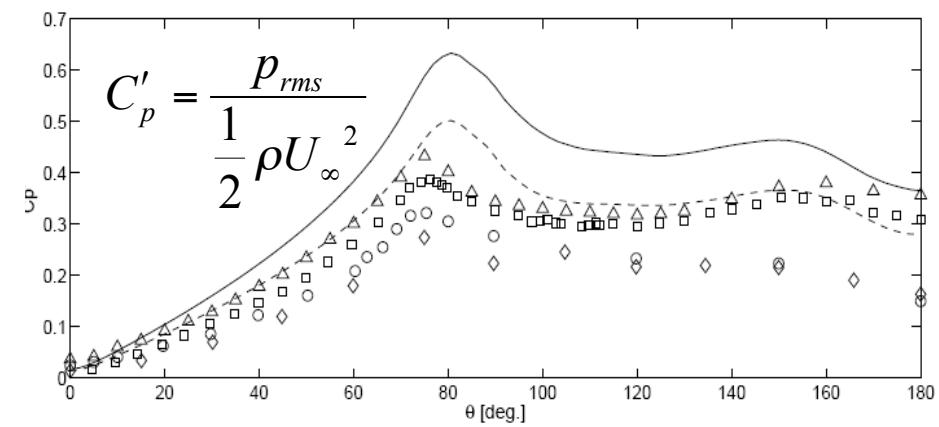
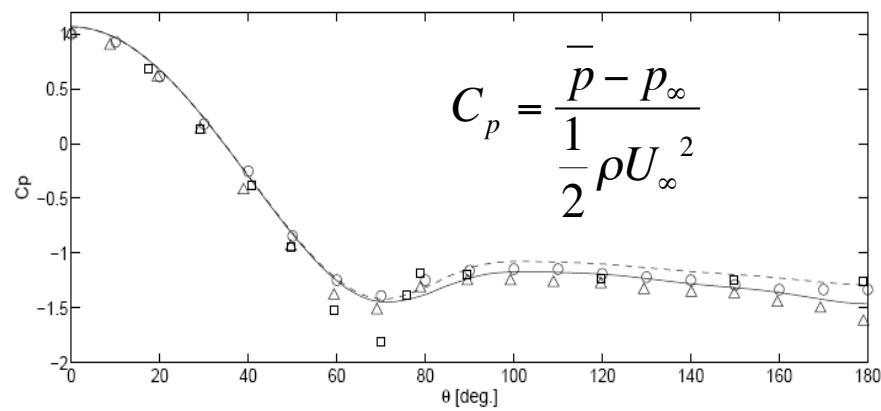
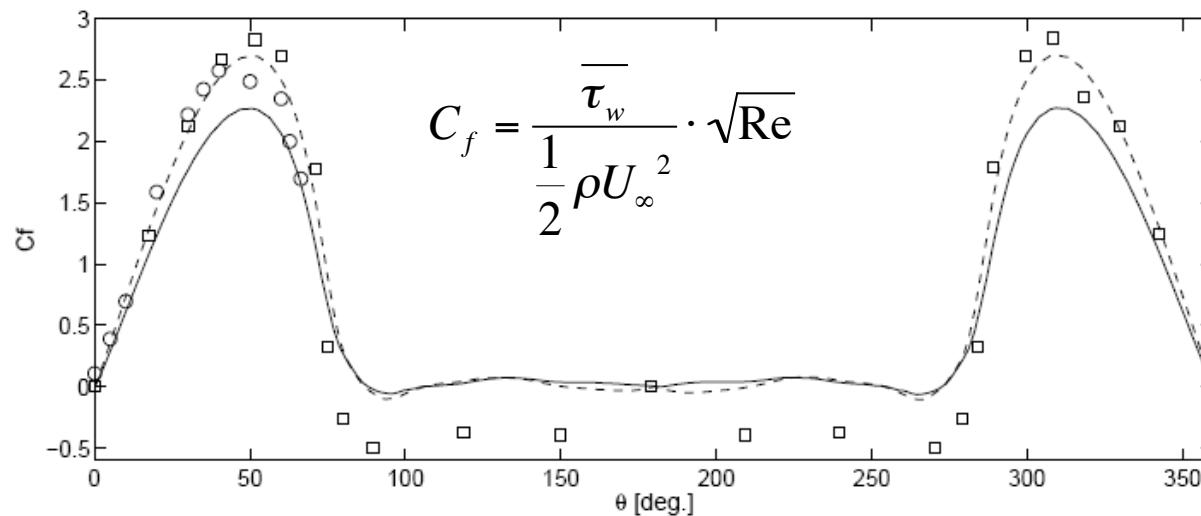
spanwise

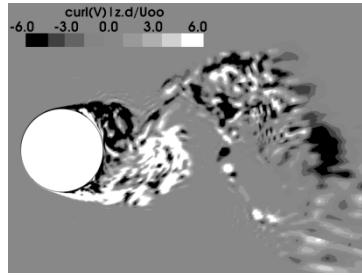
two-point correlation functions... promising for aero-acoustics



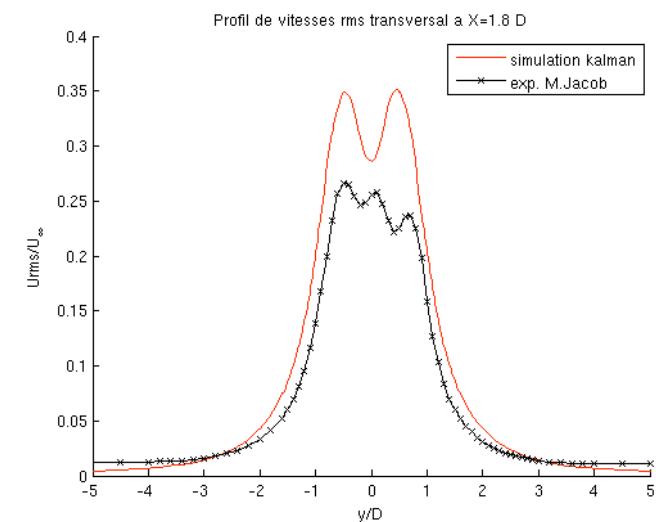
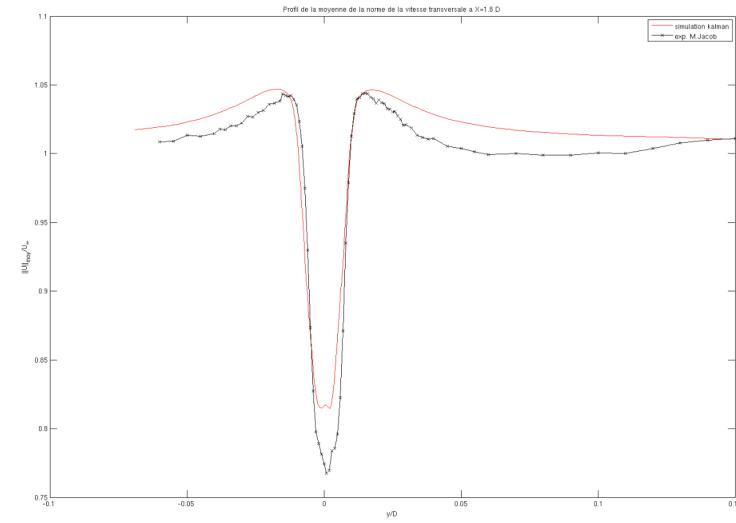
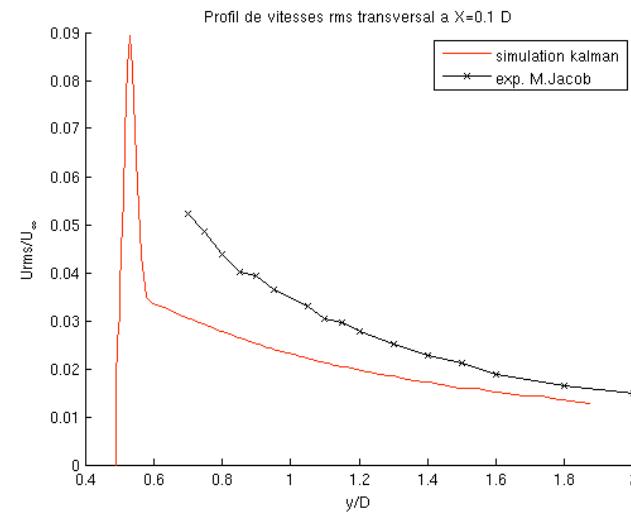
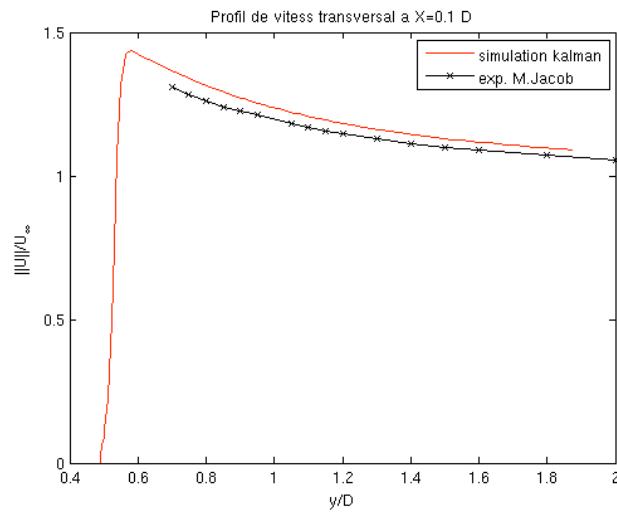
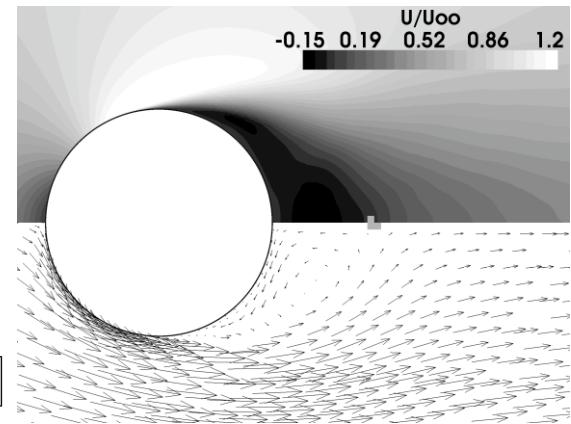
flow past a circular cylinder

Friction and pressure coefficients

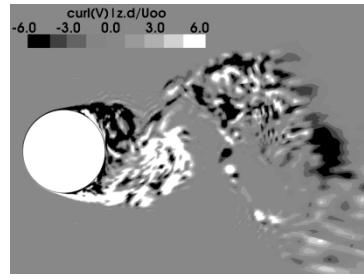




flow past a circular cylinder mean flow and turbulence intensities

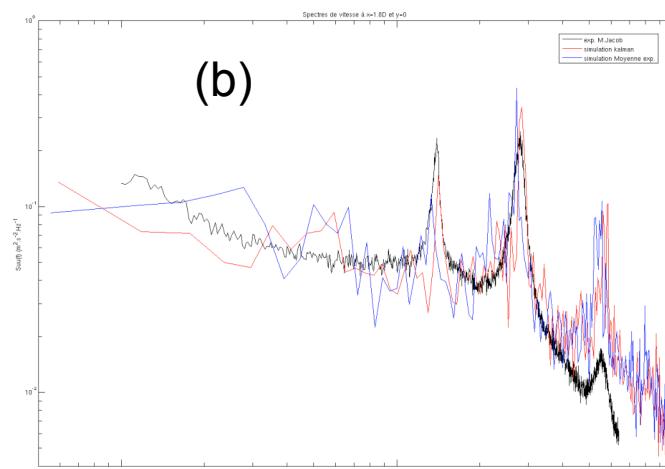
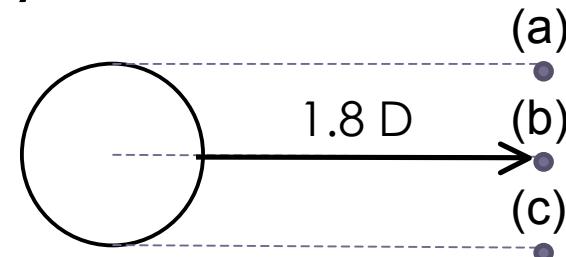
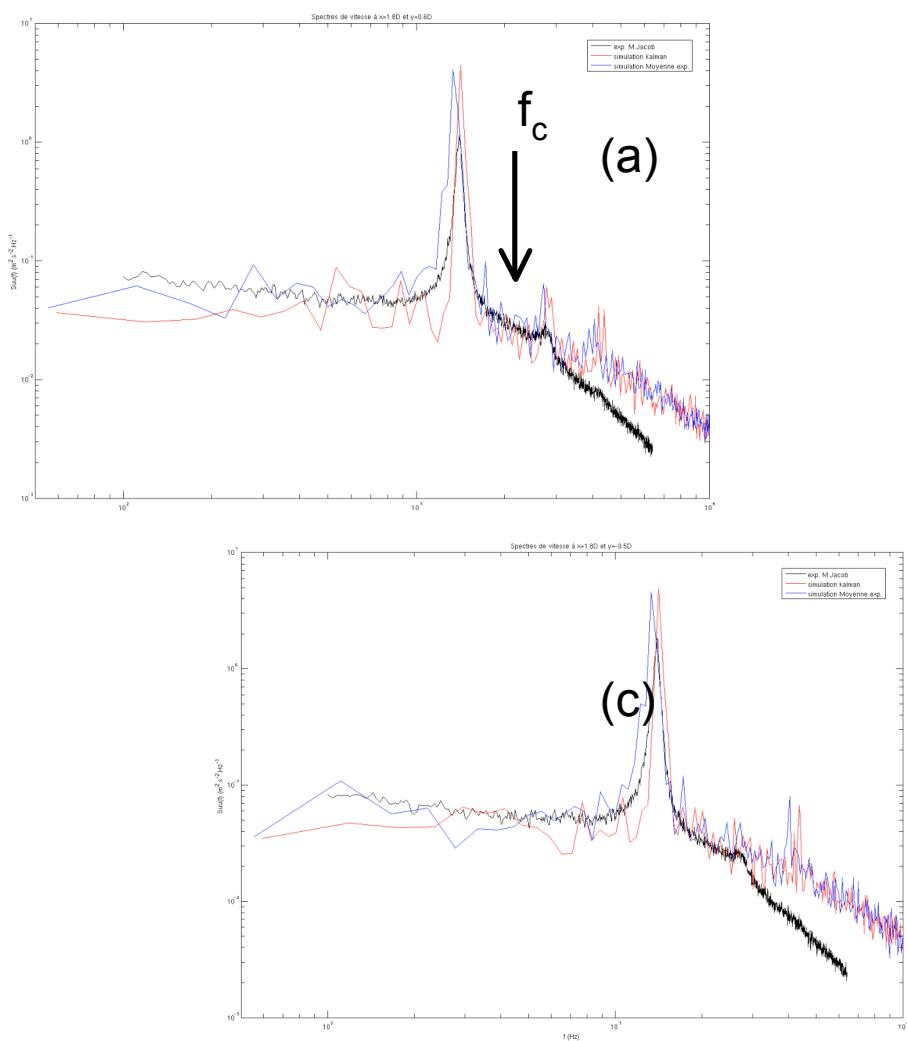


Work in progress...



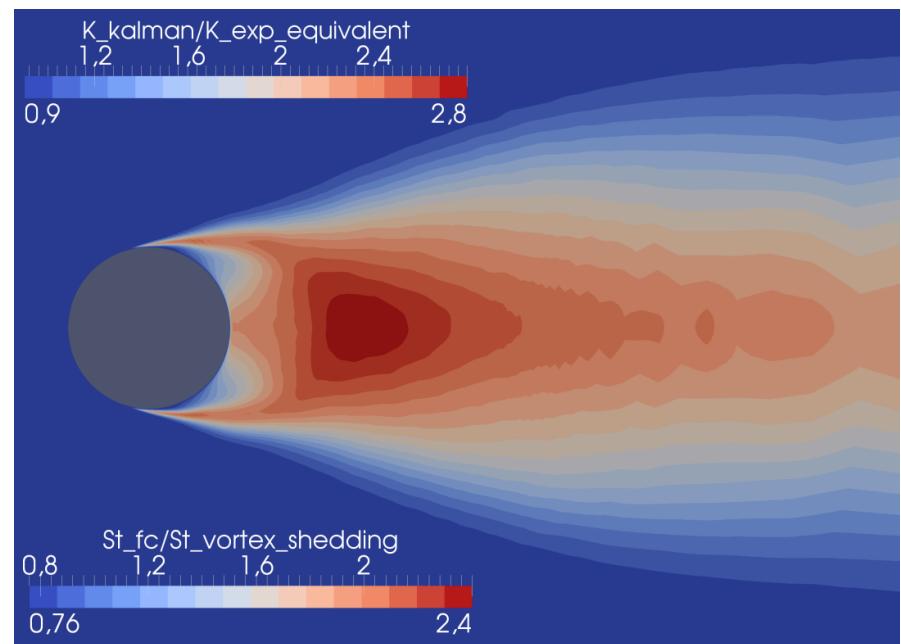
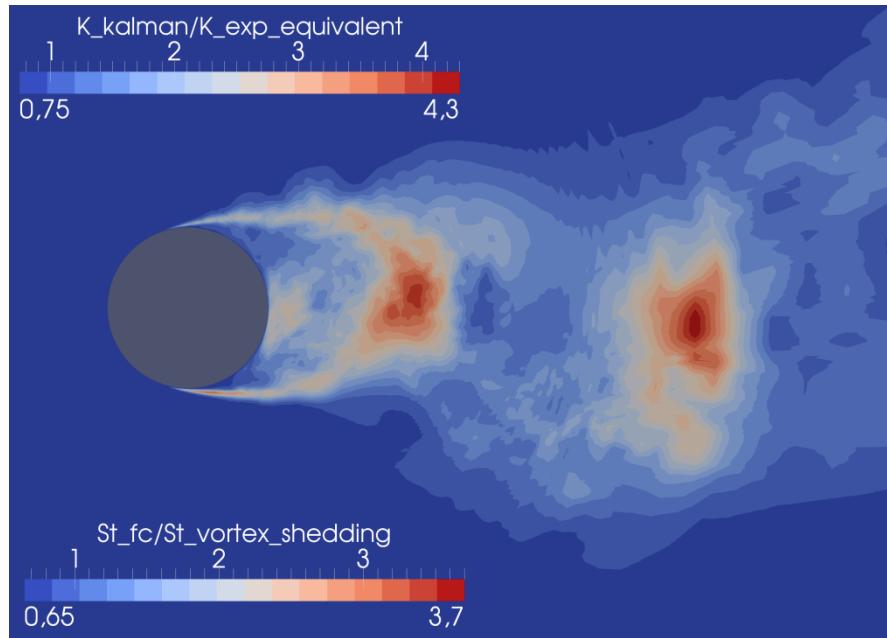
flow past a circular cylinder

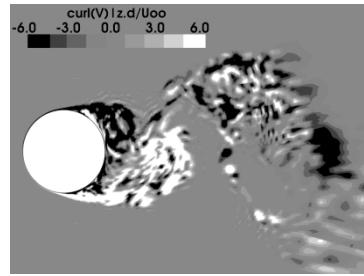
comparisons with experimental data spectra in frequency



... promising for aero-acoustics

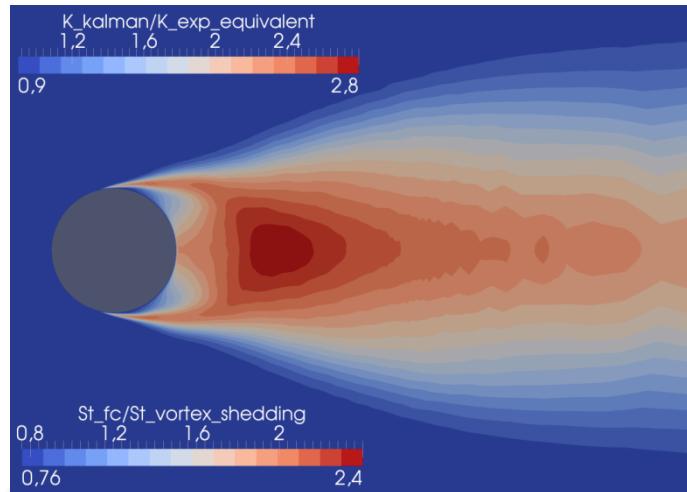
« Adaptivity » of the Kalman filter





flow past a circular cylinder

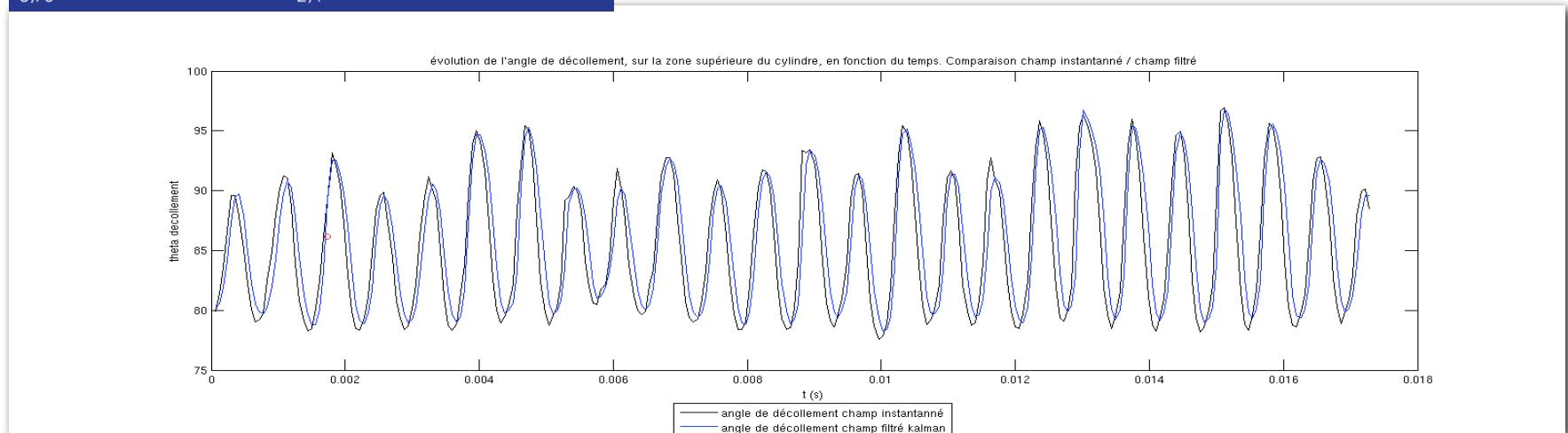
a drawback of the smoothing: phase delay



$$\Delta t / K_{Kalman}$$

$$0 < K_{Kalman} < 1$$

... make K_{Kalman} maximum in separation zone



Conclusion

from a physical viewpoint :

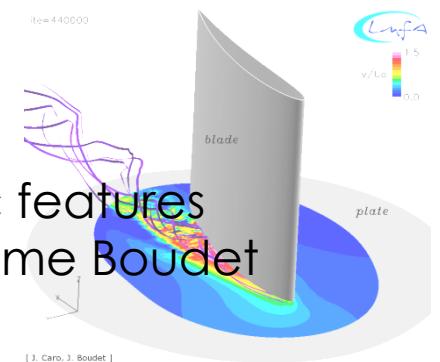
- take into account mean-flow *inhomogeneity + unsteadiness* :
SISM (no ad-hoc parameter) + (adaptive) temporal smoothing

from a numerical viewpoint :

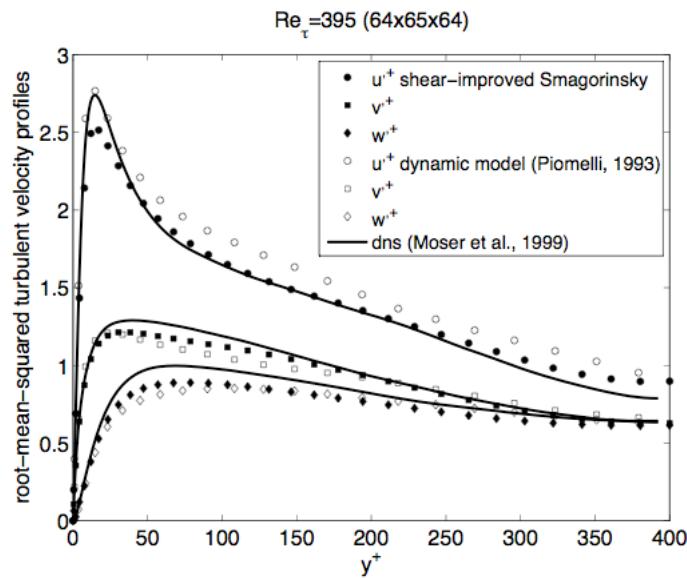
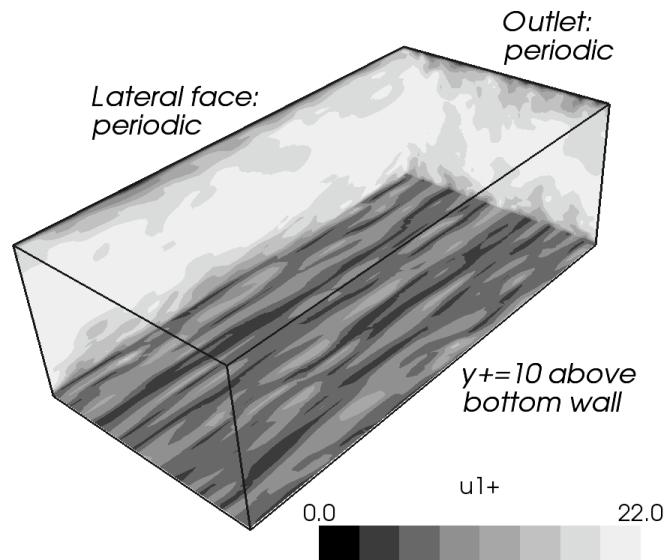
- inconditonnally stable
- low cost algorithms
- easy to parallelize + convenient for boundary conditions

To-Do list:

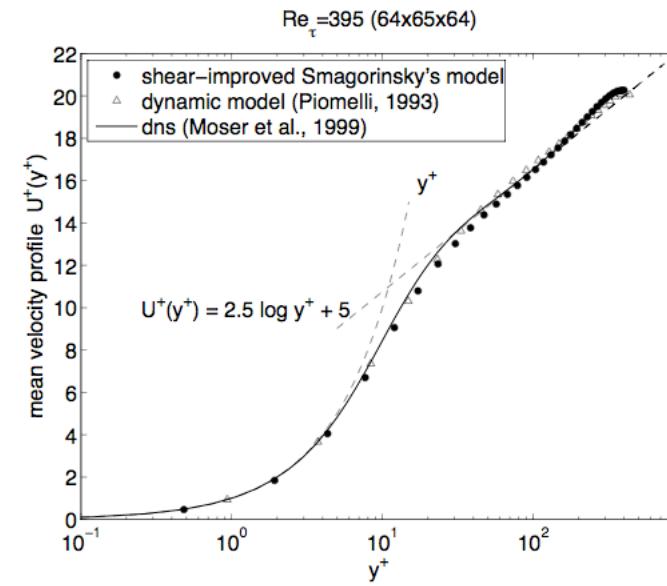
- address realistic turbo-machinery flow / aero-acoustic features
Flocon project (LMFA) : Adrien Cahuzac + Jérôme Boudet
- reduce phase delay :
 - improve Kalman filter
 - consider Lagrangian filtering (along fluid trajectory)

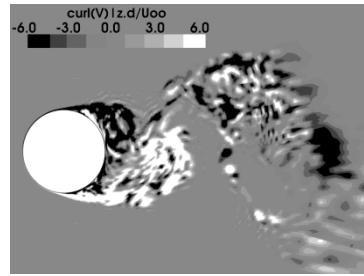


Plane channel flow (academic flow)



Lévéque et al., *J. Fluid Mech.* (2007)
Boudet et al., *J. of Therm. Science.* (2008)
Cahuzac et al. *Phys. Fluids* (2010)





flow past a circular cylinder

comparisons with experimental data

	SISM-ES	SISM-AKF	data in literature
$\langle C_D \rangle$: mean drag coefficient	1.34	1.23	1.35 ($Re_D = 4.3 \cdot 10^4$), ref. ³⁵ [1.0, 1.35] ($Re_D = 4.8 \cdot 10^4$), ref. ³⁸ [1.0, 1.3] ($Re_D = 4.8 \cdot 10^4$), ref. ³⁹ [1.1, 1.3] ($Re_D \in [10^4, 10^5]$), ref. ³⁷
C'_D : rms drag coefficient	0.09	0.065	0.16 ($Re_D = 4.3 \cdot 10^4$), ref. ³⁵ [0.08, 0.1] ($Re_D = 4.8 \cdot 10^4$), ref. ⁴⁰ [0.05, 0.1] ($Re_D \in [10^4, 10^5]$), ref. ³⁷
C'_L : rms lift coefficient	0.77	0.603	[0.45, 0.55] ($Re_D = 4.3 \cdot 10^4$), ref. ³⁵ [0.4, 0.8] ($Re_D = 4.8 \cdot 10^4$), ref. ⁴⁰ [0.6, 0.82] ($Re_D \in [10^4, 10^5]$), ref. ³⁷
St : Strouhal number	0.190	0.204	[0.18, 0.2] ($Re_D = 4.8 \cdot 10^4$), ref. ³⁸ [0.185, 0.195] ($Re_D = 6.1 \cdot 10^4$), ref. ⁴¹

flow characteristics

Mesh resolution

